

NUCLEAR MAGNETIC RESONANCE STUDIES
OF WORMLIKE MICELLES IN
POROUS MEDIA

by

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ABSTRACT

Interest of worm-like micelles (WLM) in porous media has grown in oil industries as a rock fracturing fluid due to its fluid rheology properties. Non-invasive techniques like NMR are ideal for observing and monitoring non-Newtonian fluids. This research presents data collected using NMR techniques with Cetyl trimethyl ammonium toluene (CTAT) wormlike micelles flowing through porous media. Deviations from Gaussian behavior in displacement distributions are quantified, and effects of WLM in fluid flowing through porous media was observed.

CHAPTER 1: INTRODUCTION

Non-Newtonian fluid dynamics play a major role in many industrial and environmental activities throughout society. Complex fluids can exhibit many characteristics which make their flow behavior difficult to model, such as time, temperature, and spatial dependence. Viscoelasticity, in which the fluid exhibits both solid and fluid like properties, and shear-dependent viscosity, in which the fluid properties change depending on the amount of shear applied, are examples of these behaviors [1]. Flowing these fluids through complex geometries, such as porous media, adds to the complexity of modeling the flow. Systems involving complex fluids obey conservation equations, but difficulties arise in solving these equations with the addition of multiple dependent variables. Wormlike micelles (WLM) are a class of viscoelastic fluids, and are formed by self-assembling surfactants, whose structure is comparable to long polymer chains. The research in this thesis used NMR techniques to study viscoelastic WLM flow through porous media packed beds, and compared these results to both Xanthan Gum and water. Cetyl trimethylammonium toluene (CTAT) was used in all studies and has the ability to form both spherical micelle structures, and rod-like structures at higher concentrations.

Viscoelastic fluids have uses in oil recovery, especially in shale fracturing. This technique, more commonly known as “fracking,” has been around since the 1950’s, but with advances in drilling, most notably horizontal drilling, many new opportunities for fracking have appeared throughout the United States. The fluids used in this process usually consist of a “viscosity control” polymer, such guar gum or xanthan gum, to help

with the mechanical fracturing process under high pressures. This fluid is typically recovered with the oil and either recycled on site for further use, or deposited in deep waste wells. Because of its important applicability to this ever increasing process, optimization of the fracking fluid properties has gained more interest throughout industry. Understanding of the fluid is also desired from an environmental standpoint, due to the fact that not all of the fracking fluid can be recovered [2].

Viscoelastic wormlike micelle solutions have shown a growing use in industrial processes. Hydraulic fracturing has taken advantage of the enhanced viscosity properties of WLM solutions for rock fracturing and propping in underground natural gas and oil recovery. WLM solutions also provide better permeability after fracturing sand pack pores, allowing for easier separation of fracking fluid and water. This allows for greater recovery while also reducing formation damage. WLM fracturing also requires fewer chemical additives when compared to polymer guar gum, and requires no chemical breakers. [1]

To optimize their use in these applications, it is important to understand the impact of viscoelasticity on the transport of these fluids in the subsurface. However, the subsurface is massive in scale and very heterogeneous in structure. Although model media is usually more homogenous in space than soil, it can provide information about the fluid moving through tortuous paths in a porous structure. Laboratory experiments using model porous media can shed light on the fundamental transport dynamics, a necessary foundation for input into larger and more heterogeneous systems. A true porous media by definition is a solid with many pores that provide passageway for fluids to pass through the material. A common example of this would be a household sponge.

Sandstone and shale are also considered porous media, which is the most common media where fracking occurs.

Studies in porous media using model bead packs typically measure pressure drops. Model porous media are used to study systems relevant to industrial applications; including catalysis, chromatography, and oil recovery in porous rock [3]. Difficulties in modeling flow arise due to the separation of length scales [4]. A classic approach in porous media is to model pores within the bead pack as small capillaries, with dispersion causing fluid to flow from capillary to capillary. These capillaries and dispersion act on micron length scales, depending on the pore size, but overall transport through the entire bead pack can be modeled using macroscopic Darcy's Law.

Nuclear magnetic resonance (NMR) is an effective, non-invasive, and probe free method which can gather vital data on transport dynamics in opaque porous media. In this study, NMR utilizes the interaction of hydrogen molecules' magnetic moment with a large magnetic field. NMR can provide 2D and 3D images, velocity images, and measurement of the probability distribution molecular displacement throughout the sample, requiring no assumptions about the packing network. This makes NMR a valuable tool for measuring non-Newtonian fluid flow through porous media, because it gives displacement information on the pore scale, rather than an average pressure drop over the entirety of the porous media [5].

Complex Fluids: Viscoelastic Wormlike Micelles

Wormlike micelles have shown promising uses in many fields including; natural gas and oil propagation, as drag reducing agents in heating and cooling systems, and in home care cleaning products [6]. The ability of WLM's in solution to form, break apart and reform cylindrical and spherical microstructures within a fluid can have advantageous effects in many of these industrial situations.

A fluid's dynamics can be influenced by the intermolecular and/or intramolecular forces between molecules. For a Newtonian fluid, such as water, very little of its rheology is determined by intramolecular or intermolecular forces, and a linear relationship between shear stress and shear strain with the slope being defined as the viscosity. For non-Newtonian fluids, more specifically viscoelastic wormlike micelles, both of these forces show great importance in defining the fluid's rheology. In non-Newtonian fluid, the relationship between shear stress and shear strain is not linear, and has a non-constant viscosity

Intermolecular forces within WLM can create a number of effects which impact the flow field. Due to the WLM's long chain, elastic properties, most commonly associated with polymers, can have great effect on the flow. Both tangential forces and normal forces become important due to the phenomena of micelles relieving stress with stress in a number of different ways.

WLM are commonly referred to as "living polymers," for a number of reasons. Like a polymer, a micelle can relieve physical stress that has been applied to it by reptation, caused by the random motion of molecules in fluid called Brownian motion.

Both fluids can also form entangled networks with each other at higher concentrations. Unlike a polymer, the micelle does not have a covalently bonded backbone that holds the structure together, but rather relies on intermolecular forces to hold the “polymer-like” structure together, which allows a number of more ways for the structure to relieve stress. One of these ways is that the micelle can break apart and reform into larger micelle structures in lower stress points throughout the fluid space. Another relief mechanism that micelles have over polymers is the ability to pass through each other, by pulling apart and reforming, thereby foregoing any contact stress that would arise with polymer-polymer contact [7, 8].

Micelles demonstrate a wide range of properties that make them so interesting in fluid dynamic studies. Some show shear thinning behaviors where the fluid viscosity decreases with increasing shear, while others show shear thickening behavior, where the fluid viscosity increases with increasing shear [7]. It’s these unique properties that make WLM useful as replacements for polymer solution applications. Certain concentrations of WLM studied in these experiments, cetyl trimethylammonium toluene (CTAT), has a distinctive property of changing from shear thickening to shear thinning, depending on the shear applied [Rojas], which will be discussed later. Within porous media, the tortuous nature of the fluid’s path applies a wide range of shear rates, meaning that CTAT flowing through a packed bed could show both shear thickening and shear thinning behaviors within the sample. The structure of WLM may also undergo elongational forces in porous media, which is the distribution of force along the structure. This adds to the complexity of modeling CTAT flowing through porous media, and makes MMR measurements advantageous when approaching this problem.

Modeling of viscoelastic fluids begins by describing the two ways of dissipating energy; viscous (fluid) and elastic (solid). Newton's expression for a stress tensor on an incompressible viscous fluid with a simple shear applied is:

$$\tau = -\mu(\nabla v) + (\nabla v)^+ = -\mu\dot{\gamma} \quad (1.1)$$

τ represents the shear stress tensor, which is a force per unit area applied. μ is the fluids viscosity, and v is the velocity gradient tensor. In simple shear for a Newtonian fluid, eqn 1.1 reduces to $-\mu\dot{\gamma}$, where $\dot{\gamma}$ is the shear rate .

The elastic component of the fluid can be modeled using Hooke's law for stress in an incompressible elastic solid:

$$\tau = -G(\nabla u) + (\nabla u)^+ = -G\gamma \quad (1.2)$$

u represents the displacement vector, and G is the elastic modulus. γ is called the "infinitesimal strain tensor." This is related to the rate of strain tensor by:

$$\dot{\gamma} = \frac{\partial \gamma}{\partial t} \quad (1.3)$$

It is important to note that Hooke's law is only valid for small displacements. For a viscoelastic fluid, the Maxwell model combines elastic and viscous components to define the overall stress tensor:

$$\tau + \lambda_1 \frac{\partial}{\partial t} \tau = -\eta_0 \dot{\gamma} \quad (1.4)$$

where λ_1 is a time constant that represents the relaxation time. Relaxation time is a complex subject in polymer physics, but essentially represents the amount of time the polymer takes to relieve stress under the strain experienced. With a standard polymer solution, a distribution of molecular weights, will exist in the solution. This leads to a distribution of relaxation times, because different lengths of polymer chains will take

different times to relieve stress. η_0 is the zero shear rate viscosity, or standing viscosity of the fluid. It's important to note that under rapid changes, the first term in equation (1.4) on the left hand side, which represents the viscous stress, can be neglected and the equation once integrated, reduces back to Hooke's version in equation (1.2). [9, 10]

Although Maxwell's model is good starting point for quantifying a viscoelastic fluid's response to applied shear, it does not fully describe the behavior of viscoelastic wormlike micelles. Although micelles can relieve stress in the same way as polymers, they also have the ability to break apart and reform. This creates a much smaller variance in relaxation times, due to the ability of the polymer to break apart and recombine. The lower variance in relaxation time means WLM are model polymers, such that they act as polymers that are perfectly mono dispersed, with a single relaxation time.

Porous Media

Laminar transport for porous media is considered to be both bulk fluid velocity and hydrodynamic dispersion. Mass balance for these two parameters gives the following equation:

$$\frac{\partial c}{\partial t} + \langle v \rangle \nabla c = D^* \nabla^2 c \quad (1.5)$$

where c is the concentration of fluid being tracked, $\langle v \rangle$ is the bulk fluid velocity, and D^* is the dispersion coefficient. Dispersion follows Brownian motion characteristics, where

$$\langle z^2(t) \rangle = 2D^* t \quad (1.6)$$

in which $\langle z^2(t) \rangle$ is the variance of the fluids position.

Porous media can be modeled as bundles of tiny capillaries, with laminar flow.

The Navier-Stokes conservation equation in cylindrical coordinates for flow in a z direction in a cylindrical capillary is:

$$\rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial p}{\partial z} - \left[\frac{1}{r} \frac{\partial}{\partial r} (r \tau_{rz}) + \frac{1}{r} \frac{\partial}{\partial \theta} \tau_{\theta z} + \frac{\partial}{\partial z} \tau_{zz} \right] + \rho g_z \quad (1.7)$$

With the definition that $\tau_{rz} = -\mu \left[\frac{\partial v_r}{\partial z} + \frac{\partial v_z}{\partial r} \right]$, and by assuming that the flow is steady, unidirectional, axisymmetric, and fully developed, equation (1.5) becomes:

$$\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) = \frac{1}{\mu} \frac{\partial p}{\partial z} \quad (1.8)$$

By applying the boundary conditions of no slip and a finite velocity at the center of the pipe, this equation can be integrated to get:

$$v_z = -\frac{1}{4\mu} \frac{\partial p}{\partial z} (R^2 - r^2) \quad (1.9)$$

Where R is the radius of the pipe. By integrating v_z over the entire radius of the pipe, the average velocity, $v_{z \text{ avg}}$, can be calculated. The max velocity, $v_{z \text{ max}}$, can also be obtained by noting that the fluid moves fastest in the very center of the pipe.

$$v_{z \text{ avg}} = \frac{1}{\pi R^2} \int_0^R v_z 2\pi r dr = 0.5 v_{z \text{ max}} \quad (1.10)$$

$$v_{z \text{ avg}} = \frac{D^2}{32\mu} \left(\frac{\partial p}{\partial z} \right) \quad (1.11)$$

By solving for $\left(\frac{\partial p}{\partial z} \right)$, and setting this to the pressure drop over the entire length of the flow, a relationship between a measured pressure drop and the average velocity is found.

$$\Delta P = \frac{(32\mu L v_{z \text{ avg}})}{D^2} \quad (1.12)$$

By assuming that porous media is essentially a large collection of capillary tubes that all flow in laminar way, also known as Hagen-Poiseuille flow, the Carman-Kozeny

equation can be found by redefining the geometry the fluid flows through. This assumption is simply made by taking all the pathways the fluid can take through the porous media as laminar flowing cylindrical pipes [Bird]. For porous media constructed of monodisperse spherical beads, such as that used in this thesis, the Carman-Kozeny equation becomes:

$$\frac{\Delta P}{L} = \frac{180v_{avg}\mu(1-\varepsilon)^2}{D_p^2\varepsilon^3} \quad (1.13)$$

with D_p as the bead diameter, and ε as the void fraction or porosity of the media.

This equation is ideal for use in the lab because pressure change from the start to the end of the bead pack can be easily measured using simple pressure transducers[9]. With pressure drop data, the velocity can be found, although this velocity is average over the bead pack. With a complex fluid, spatial dependence of material properties comes into play within the Navier Stokes equation. NMR can measure probabilities of molecular displacement with the pulse gradient spin echo (PGSE) sequence. By doing this, velocity data is collected without any further assumptions on the heterogeneity of the bead pack, or rheological properties of the fluid [11-17].

CHAPTER 2: INTRODUCTION TO NUCLEAR MAGNETIC RESONANCE (NMR)

Magnetic resonance is a powerful non-invasive analytical tool used by many industries today. By taking advantage of quantum mechanical properties of nuclei with magnetic moments, most notably hydrogen in this thesis, NMR can provide data on molecular structure, spatial geometry, and/or flow dynamics. In medicine, Magnetic Resonance Imaging (MRI) is used to image tissue to check for problems such as tears, liaisons, and tumors with resolutions typically less than a millimeter. MRM uses magnetic fields to spatially encode hydrogen spins, and determine fluid motion in complex systems with resolution typically less than 100 μm [11].

Quantum Mechanics of Hydrogen

In this section, properties of hydrogen will be discussed as it is the nuclei observed within the MRM studies in this thesis.

Due to the distribution of charges, each nucleus has an angular momentum (J), and a magnetic moment (μ). The angular momentum of the nuclei is defined by the spin angular quantum number (I). For hydrogen, this number is $1/2$, which means that each nucleus exist in one of two stable energy states, spin $+1/2$ or $-1/2$, or spin up or spin down, respectively.

In the presence of a large magnetic field B_o , the nuclei processes at a frequency caused by the torque on the magnetic moment μ . This precession is at the Larmor frequency ω_o and γ is the gyromagnetic ratio.

$$\omega_o = \gamma B_o \quad (2.1)$$

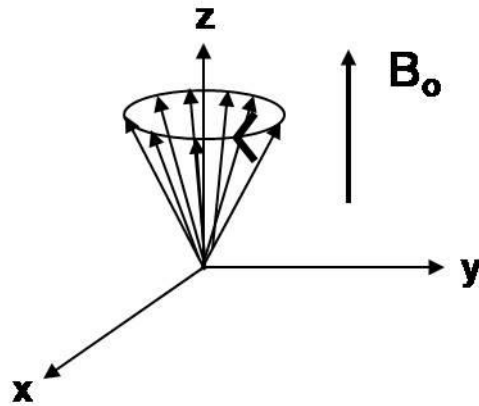


Figure 2.1: The magnetic moment of a hydrogen atom precessing around the z-axis when applied to magnetic field

The nuclei, or “spins,” will also align either parallel or antiparallel to the applied field, B_0 . Due to having slightly more spins in the parallel position, there is a net magnetization the direction of the applied magnetic field, which can be manipulated to give signals that lead to imaging and velocity measurements.

Without any applied magnetic fields on a sample containing hydrogen nuclei, the magnetic moments are randomly oriented in every direction.



In the absence of a magnetic field, the spins are randomly oriented

In the presence of a static magnetic field B_0 , the spins are aligned parallel or antiparallel to B_0 .

Figure 2.2: Orientation of magnetic moments with and without applied magnetic field.

The summation of these magnetic moments is zero without an applied field. When a constant magnetic field (B_0) is applied to the sample, the molecules align in either spin up state, or spin down state, but there is energy difference between the two states, shown in equation 2.2.

$$\Delta E = \frac{\mu B_0}{I} \quad (2.2)$$

The probability of a molecule being aligned with B_0 , which is the low energy state, is given by the Boltzman's distribution.

$$P = \exp\left(\frac{\gamma \hbar B}{k_b T}\right) = \exp\left(\frac{E}{k_b T}\right) \quad (2.3)$$

where γ is the gyromagnetic ratio, \hbar is Planck's constant ($1.0546 \cdot 10^{-34}$ J sec/rad), k is Boltzmann's constant ($1.3805 \cdot 10^{-23}$ J/K), and T is temperature in Kelvin. Due to nuclei having a slightly larger probability of being aligned with the B_0 field, MRM is possible.

Due to the nuclei having a charge and spinning, a dipole moment is observed. The magnetic dipole moment of the hydrogen in a magnetic field is

$$\mu = \gamma \hbar I \quad (2.4)$$

This moment is analogous to a compass needle spinning in an applied magnetic field, which is an example of the Einstein-de Haas effect. This can be related to the conservation of momentum, and how the net magnetization evolves in an applied magnetic field.

$$\frac{dM}{dt} = -\gamma B \times M \quad (2.5)$$

The classical idea of magnetic angular moments can be used to explain the quantum idea of magnetic moments by creating spin ensembles that experience the same

applied magnetic field, and therefore sum their respective magnetic dipole moments into one overall moment ($M = \sum \mu$). This now allows us to think of the quantum angular moments as one single vector of magnetization, where the magnitude of this vector is determined by the sum of all spins with respective μ .

Another concept that helps with the transition between classical and quantum thinking is the application of a rotating frame of reference.

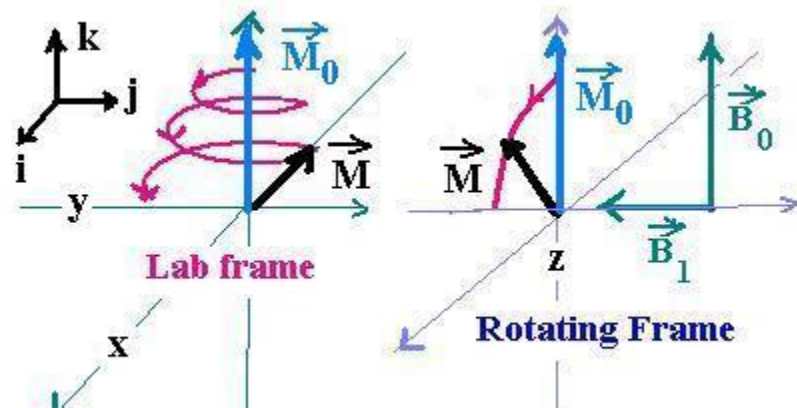


Figure 2.3: Magnetization shown tipping down into the transverse plane when excited by a B_1 field. In the lab frame, the magnetization precesses around the z axis, while in the rotating frame M can be thought of as a stationary vector.

The reference frame is a Cartesian coordinate system in which B_0 is aligned with the z direction, and the entire coordinate system is rotating at the appropriate Larmor frequency defined by equation (2.2). Within this rotating frame, the net magnetization appear as a stationary vector.

Radio Frequency Excitation

Now that the rotating frame has been defined, manipulating or “tipping” the net magnetization into the transverse plane where it can be detected is done by applying an oscillating magnetic field called B_1 . This field is applied perpendicular to B_0 and oscillates at the Larmor frequency, and therefore can be thought of as coming in along the x or y axis in the rotating frame. With this additional field, equation (2.5) becomes:

$$\frac{dM}{dt} = -\gamma M \times B_1 \quad (2.6)$$

With the applied magnetic field B_1 defined as:

$$B_1(t) = B_1 \cos(\omega_0 t) \mathbf{i} - B_1 \sin(\omega_0 t) \mathbf{j} \quad (2.7)$$

Here, \mathbf{i} and \mathbf{j} can be thought of the x and y coordinates, or the transverse coordinates. Now that we know how B_1 rotates around the B_0 , the net magnetization’s oscillation can also be defined in the non-rotating Cartesian system by plugging equation (2.7) into equation (2.6).

$$\frac{dM_x}{dt} = -\gamma [M_y B_0 + M_z B_1 \sin(\omega_0 t)] \quad (2.8)$$

$$\frac{dM_y}{dt} = -\gamma [M_z B_1 \cos(\omega_0 t) - M_x B_0] \quad (2.9)$$

$$\frac{dM_z}{dt} = -\gamma [M_x B_1 \sin(\omega_0 t) - M_y B_1 \cos(\omega_0 t)] \quad (2.10)$$

Applying the boundary condition $\omega_1 = \gamma B_1$ and the initial condition $M(t) = M_0 \mathbf{k}$, the above equations can be solved to become:

$$M_x = M_0 \sin(\omega_0 t) \sin(\omega_1 t) \quad (2.11)$$

$$M_y = M_0 \cos(\omega_0 t) \sin(\omega_1 t) \quad (2.12)$$

$$M_z = M_o \cos(\omega_1 t) \quad (2.13)$$

These equations show that the net magnetization precesses about B_1 . In the rotating frame, the magnetization can be thought of as tipping down into the transverse plane. It should be noted that the above equations ignore relaxation effects, which are discussed later [11, 18, 19].

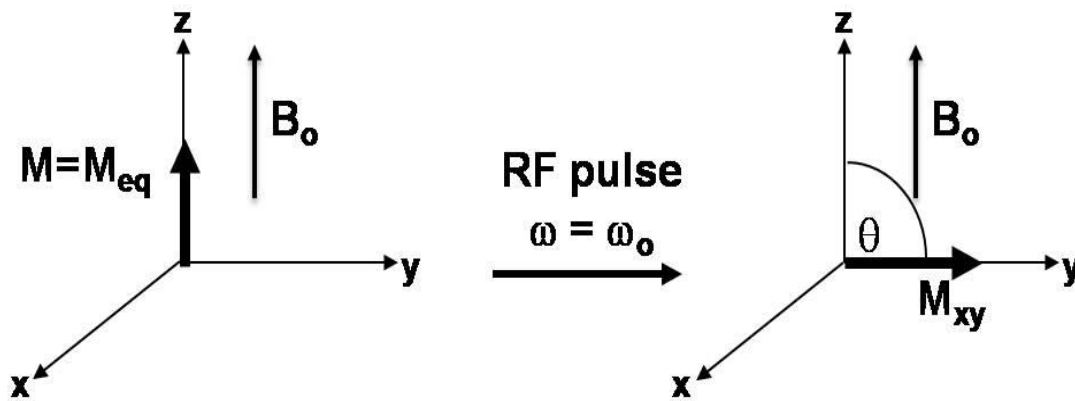


Figure 2.4: Effect of the rf pulse on the net magnetization

In order to apply the oscillating B_1 field that tips the net magnetization into the transverse plane where signal can be detected, a radio frequency coil is used since the energy needed to excite spins, between energy states is in the radio frequency range for large superconducting magnet.

The angle at which the magnetization is tilted is controlled by the duration and strength of the B_1 field termed the radio frequency (rf) pulse, is equation (2.13):

$$\theta = \gamma B_1 t_p \quad (2.14)$$

Where θ is the tilt angle in degrees, B_1 is the amplitude of the electromagnetic field due to the rf pulse, and t_p is the pulse duration.

A diagram of this action is presented in figure 3. Once the net magnetization is aligned in the transverse plane it precesses, producing a voltage signal referred to as the Free Induction Decay (FID) [11, 19].

Relaxation

The magnetization will return to thermal equilibrium and align back with B_0 over a period of time termed the relaxation time. This relaxation is classified in two categories, T_1 and T_2 .

T_1 classifies the phenomena of the net magnetization of the sample returning to equilibrium in the longitudinal plane aligned with B_0 . This happens by protons releasing energy to their surrounding lattice. Due to this effect, T_1 is the spin-lattice relaxation, or longitudinal relaxation. The governing equation for this is shown in equation (2.15):

$$\frac{dM_z}{dt} = \frac{-(M_z - M_0)}{T_1} \quad (2.15)$$

Solving this equation yields:

$$M_z(t) = M_z(0) + M_0(1 - \exp\left(-\frac{t}{T_1}\right)) \quad (2.16)$$

Where M_z is the longitudinal component of the magnetization and M_0 is the net magnetization in the applied B_0 field. T_1 is correlated towards the “fast” molecular motions, and becomes highly dependent on a sample’s phase, viscosity, temperature, and spin frequency. A typical T_1 may fall between 0.1 to 10 seconds. In some cases, such as solids, T_1 may become very high due to the restricted molecular mobility. For example, T_1 for diamond is measured on the order of weeks rather than seconds.

A sample's T_1 is generally the restricting parameter when performing experiments. A rule of thumb within NMR is that pulse sequences must wait $5 T_1$ intervals before running again to ensure all spins return to equilibrium. Due to this, longer T_1 can increase an experiments time drastically. To combat this, a common relaxation agent called Magnevist is added to samples which greatly increases the lattice interactions. Magnevist essentially lowers T_1 by creating relaxation sites.

T_2 relaxation is dephasing of the net magnetization of hydrogen while in the x-y plane. It is termed spin-spin relaxation since it is due to energy exchange between spins. T_2 is typically less than T_1 , and is the governing time restraint on data collection window for experiments. As described previously, a net magnetization is caused by a state of phase coherence between spins. Therefore, when these spins start to dephase, or lose coherence, the net magnetization decreases. A common visualization of T_2 is runners on a race track. At the start of the race, all runners are lined up, but as the race progresses, they spread out over time. T_2 happens very rapidly, especially in porous media where spins interact with pore walls. Ways to combat this process and collect signal before decay of the net magnetization will be discussed later. The evolution of the magnetization with T_2 is:

$$\frac{dM_{x,y}}{dt} = \frac{-M_{x,y}}{T_2} \quad (2.17)$$

Solving the equation yields:

$$M_{x,y}(t) = M_{x,y}(0)e^{-t/T_2} \quad (2.18)$$

Although ideally the signal decays away purely due to T_1 and T_2 , inhomogenaties in the magnetic field and/or rf pulses cause additional T_2 relaxation. To account for this, the

decay of the FID T_2 is usually referred to as T_2^* , meaning that any extra effects on the relaxation time are contained in the given number [19].

Bloch Equations

Adding the relaxation effects from equations 2.17 and 2.18, to equation 2.5 gives the Bloch equations, named after their founder physicist Felix Bloch. The result determines the net magnetization acts when an excitation pulse is applied, and how it evolves due to both T_1 and T_2 :

$$\frac{dM_x}{dt} = \gamma M_y \left(B_0 - \frac{\omega}{\gamma} \right) - \frac{M_x}{T_2} \quad (2.19)$$

$$\frac{dM_y}{dt} = \gamma B_1 - \gamma M_x \left(B_0 - \frac{\omega}{\gamma} \right) - \frac{M_y}{T_2} \quad (2.20)$$

$$\frac{dM_z}{dt} = -\gamma M_y B_1 - \frac{(M_z - M_0)}{T_1} \quad (2.21)$$

Signal Detection

Detecting NMR signal is governed by Faraday's Law, which predicts how a magnetic field will interact with an electric circuit to produce an electromagnetic force (EMF). In this case, the EMF is the result of the processing net magnetization of the excited protons as they move in the rf coil.

The signal in a NMR experiment is the sum of magnetization, from the ensemble of spins in the sample. These ensembles can be thought of as groups of hydrogens that see the same effective gradient within the sample, and therefore will return identical

signals back, resulting in one summed signal for all hydrogens within i^{th} ensemble. The signal (S) for an NMR experiment in a volume element can be defined as:

$$dS(G, t) = \rho(r)dV e^{i\gamma Bt} \quad (2.22)$$

where $\rho(r)$ at location (r) is defined as the spin density, and dV is the finite volume element. These spin ensembles are subject to the thermodynamic principles of displacement, most notably Brownian motion. Random motions of spins causes attenuation of S , leading to a Gaussian distribution in displacements once averaged, and bulk motions are accounted through bulk phase shifts that will be discussed later.

The amplitude of the signal represents the spin density of the sample's particular area under measurement. Signal is collected as a function of time, where the amplitude decays away due to relaxation. To take data into the frequency domain, Fourier transforms are required. The Fourier relationship between frequency domain (k) and time domain (t) is:

$$F(k) = \int f(t)e^{-ikt} dt \quad (2.24)$$

$$f(t) = \int F(k)e^{ikt} dk \quad (2.25)$$

Due to the low signal to noise nature of NMR which is best seen in the above discussion of the Boltzman's distribution of spins, MR experiments, or sequences, are commonly repeated many times and averaged to cancel out any noise contained within the data. This, along with the spin ensemble averaging mentioned in the above paragraph means that NMR experiments are double averaged, once in space, and again in time. This double averaging can lead to lengthy experiment times, which varied from 15 minutes, to 24 hours in the experiments performed in this body of work. Due to this, NMR shows

many restraints in the measuring of transient or short time dependent systems, and works much better for steady state and fully developed processes[11, 20].

CHAPTER 3: ADVANCED NMR TOPICS: GRADIENTS, SEQUENCES, IMAGING, AND MOTION TRACKING

In the previous chapter, the basics of excitation, relaxation, and signal detection were explained. This chapter will discuss more advanced topics, focusing on spatially dependent magnetic field gradients used to create 1-D and 2-D images, and how sequences for gradients can measure displacement over set periods of time, leading to velocity measurements.

All NMR setups use a series of solenoids to generate and control the magnetic field within the apparatus. The outer, largest coil, is used to create a dominating B_o field, which is aligned in the vertical (z axis) direction, and has varying amplitudes. The magnetic field used in these experiments was a constant 7 T (Tesla) field. As a reference the earth's magnetic field ranges between 25 and 65 mT. A 7T field translates into a 300 MHz Larmor frequency. A smaller, inner coil is used to apply spatially varying gradients to the magnetic field. Although the magnitude of the applied gradients from this coil are drastically smaller than the outer coil, these gradients are strong enough to encode the proton's spin to its position [11].

With application of a constant gradient, the effective magnetic field becomes equation (3.1):

$$B_{eff} = B_o + \vec{G} \cdot \vec{r} \quad (3.1)$$

The terms are now represented as vectors to show the spatial dependence. B_o is the strong field aligned along the z axis, discussed in chapter 2. It should be noted that this term is always the strongest, and dominates the hydrogen quantum mechanics in terms of

spin and Larmor frequency. \vec{G} is the applied spatial gradient from the inner coil, and can be applied in any direction. This term is multiplied by a spatial coordinate, \vec{r} , meaning that the gradient seen by a particular hydrogen ensemble located at one point will see a different magnitude of gradient than a hydrogen ensemble located at another point in space.

This additional gradient also changes the frequency of spins as a function of position with the Larmor frequency relationship, equation (2.1).

$$\omega(r) = \gamma(B_{eff}) = \gamma(B_o + \vec{G} \cdot \vec{r}) \quad (3.2)$$

As seen above, with the appropriate gradient applications, hydrogen ensembles frequency can be encoded to its placement in the sample. Gradient applications vary in length, depending on the desired information from the sample. For example, a simple 2-D image of an object uses gradients that only encode for space. Gradients can also be used to measure hydrogen ensemble displacement, which paired with known timings in the gradient applications can lead to velocity and diffusion measurements. Gradient applications can even be stacked together in experiments, leading to data that has multiple dependencies, allowing for experiments such as 2-D velocity images. A few of these techniques will be discussed later on, mostly focusing on imaging and displacement techniques used in the body of work for water and WLM flows in porous media.

Slice Selection

This inverse relationship between time and frequency is key to understanding how rf pulses are applied. To specify a bandwidth, or range of frequencies excited, the length

and shape of the rf pulse is adjusted. A long rf pulse will excite a narrow range of frequencies, and a short r.f pulse will excite a wide range of frequencies. Rf pulses use adjectives such as hard and soft to quantify the shape of the pulse. Generally, a hard pulse is square in shape, whereas a soft pulse has a sinc function shape. Along with application of a gradient, this can selectively excite a slice within the sample.

k-space

As discussed above in chapter 2, the relationship between the time and frequency domain is what makes NMR imaging possible. This frequency domain is referred to as k-space, which is the conjugate of position. K-space, is a 2D Fourier transform of a 2-D image. k's dependence on a spin's phase is shown in equation (3.3).

$$k = \frac{\gamma G t}{2\pi} \quad (3.3)$$

To collect signal from different points within k-space, gradient sequences are used to traverse the two dimensions: phase and read, or k_y and k_x , respectively. The gradients used to do this are commonly referred to as the read gradient (G_r) and phase gradient (G_p). A diagram example of how k space is sampled is shown below.

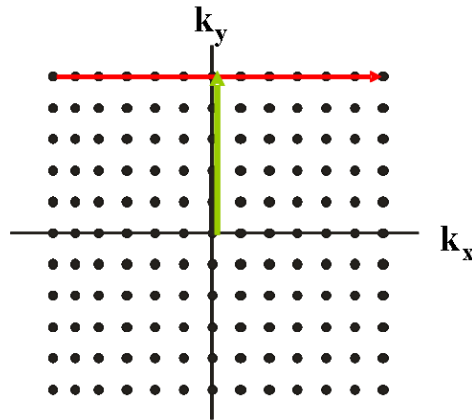


Figure 3.1: The green arrow represents traversing in phase direction, with the red arrow traversing in the read direction.

In this example, a simple 1-D image is being measured. Within the sequence a phase gradient is applied directly after the magnetization is tipped into the transverse plane. This constant gradient changes the magnetic field linearly in space, and changes the hydrogens' frequency in correlation with their position within the sample, causing them to become out of phase, i.e. the further away the hydrogens are from the center of the sample, the more out of phase their respective magnetization vectors become. This process is commonly referred to as phase encoding, and the phase shifts are dependent on the amplitude of the gradient applied. The second dimension is sampled using the read gradient. Unlike the phase encoding gradient, where a gradient of chosen amplitude is applied to select a specific k_{ph} value, the read gradient is a constant gradient applied during collection of the echo. This is commonly referred to as frequency encoding. The time and amplitude dependence for how the read and phase gradients traverse through their respective space is shown below:

$$\Delta k_{read} = -\gamma G_r \Delta \tau_{read} \quad (3.4)$$

$$\Delta k_{phase} = -\gamma \Delta G_p \tau_{phase} \quad (3.5)$$

τ represents the time each gradient is applied. Most often in frequency encoding, k_{read} , is controlled by varying τ_{read} , whereas phase encoding is controlled by varying either ΔG_p or τ_{phase} . A figure of the described sequence is shown below:

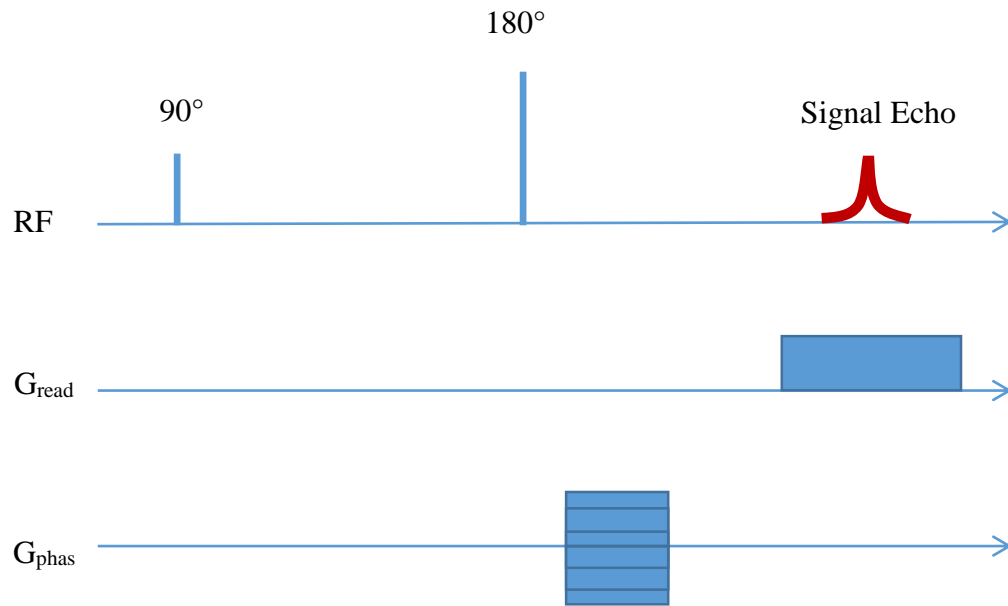


Figure 3.2: 1-D imaging sequence. G_{phase} is applied first, with varying amplitudes each sequence, while G_{read} is a constant amplitude and applied during signal collection.

Due to the phase space being selected once per sequence, and all read points are collected within that respected phase line, the time of experiment is highly dependent on the number of phase lines sampled. The number of phase lines and read lines sampled is referred to as the resolution, and for a 2-D image the resolution can be thought of the same way as a camera or a display screens respective resolution works. Due to the fact that imaging software used for these experiments takes advantage of Fast Fourier

Transform (FFT) algorithms, data matrix sizes of 2^n are best [11]. A common square 2-D image may have a matrix size of 256×256 , which would correspond to 256 phase encoding lines and 256 read encoding lines, respectively. For oblong shapes, such as a tube with fluid, an image would most likely be 128×256 . This is done to keep the pixel size the same in both directions.

The phase matrix size also varies the length of experiment, which can have high importance if the sample has any time dependent properties. Because only one line in the phase direction can be read off in each sequence, a relaxation period must be applied before the next sequence is run. As mentioned before, $5T_1$ must pass before the next sequence can be applied to the sample. Therefore, increasing, or decreasing, the number of phase lines has a great effect on the length of the experiment. Going from 256 to 128 points in the phase direction will cut the experiment time in half, and can be very useful when imaging oblong shapes.

To connect the signal collected from sampling k -space in the above sequence, to the overall goal of imaging, which is finding the spin density at certain position requires a Fourier transform. This is done by writing equations (2.24) and (2.25) in terms of the spatial component r . The resulting equations show the relationship between the signal gathered, and the spin density in space $\rho(r)$:

$$S(k) = \int \rho(r) \exp[i2\pi k \cdot r] dr \quad (3.6)$$

$$\rho(r) = \int S(k) \exp[-i2\pi k \cdot r] dk \quad (3.7)$$

Motion Tracking: q-space, Diffusion, and Propagators

Much in the same way position is measured using k-space, motion is tracked using gradient applications in pulse sequences. We similarly call the reciprocal space to displacement q-space. A good analogy for how bulk motion is tracked in NMR is taking pictures of fish in water. Imagine standing above the water and taking two pictures, separated by a time, Δ . When these two pictures are analyzed, it's seen that the fish has moved a distance, $r-r'$. By knowing the distance, and the time between the two pictures, a velocity can be obtained for that particular fish. Similarly, NMR can track movement by getting signal from spins at two different times, and knowing the separation between the two signal acquisitions.

In this body of work, the pulsed gradient stimulated echo experiment (PGStE), shown in figure 3.3, is used to find effective self-diffusion coefficients, as well as the overall propagator. This pulse sequence starts with a 90° RF pulse which brings the spins into the transverse plane. The dephasing gradient pulse winds a helical phase shift the spin isochromats in the direction of the applied gradient. This square magnetic gradient pulse is applied for a duration δ , with magnitude g in the direction that displacements are to be measured. Another 90° RF pulse stores the magnetization in the transverse plane, saving the magnetization from T_2 decay. A spoiler gradient is applied while the magnetization is in the transverse plane to dephase any remaining signal. The importance of this is so that the third 90° pulse affects all spin isochromats in the same way, pulling them again into the transverse plane. This third 90° pulse reverses the direction of precession of the spin isochromats from their original precession, making the first

gradient pulse effectively negative. The rewind gradient pulse is applied after a time Δ from the start of the dephasing gradient pulse. The rewind gradient pulse, equal in magnitude and duration to the dephasing gradient pulse, reverses the dephasing. Signal is acquired at the spin echo. Because the entire echo is acquired, the echo contains information on the spectral frequencies within the sample [11, 18, 21-24].

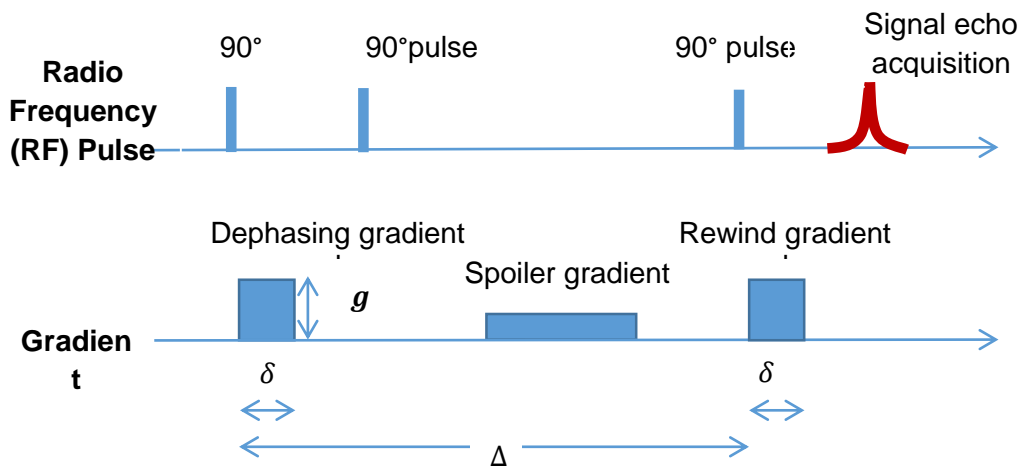


Figure 3.3: PGStE sequence used to track spin ensemble movement. The gradient encodes the spin ensembles for position, then waits Δ , and unwinds with the same gradient. The resulting phase shift and attenuation then shows movement in the sample.

The PGStE sequence is ran multiple times with incremental gradient values, with the same effect on experimental times that the phase encoding gradient had in k-space.

The Bloch-Torrey approach to the analysis of translational motion of spin isochromats is specific to systems undergoing only diffusion and flow [11]. The gradient moments approach assumes coherent motion. Both of these methods do not allow for quantitative analysis of general motion. However, it is possible to look at the echo signal as an accumulation of phase shifts from spin isochromats to analyze general motion. This

is valid when the narrow gradient pulse approximation can be made, $\delta \ll \Delta$, such that spins don't move considerably over the course of the applied gradient.

$$E(\mathbf{g}, \Delta) = \int \rho(\mathbf{r}) \int P(\mathbf{r}|\mathbf{r}', \Delta) \exp(i\gamma\delta\mathbf{g} \cdot [\mathbf{r} - \mathbf{r}']) d\mathbf{r}' d\mathbf{r} \quad (3.8)$$

Equation (3.8) states that the PGSE echo signal, when applying a gradient, \mathbf{g} , and using an observation time, Δ , is equal to the sum of all signal phase shifts from all spins due to displacements from their initial locations \mathbf{r} to their final locations \mathbf{r}' over the observation time

In order to define the signal space in which the propagator is sampled, the variable \mathbf{q} is defined: $\mathbf{q} = \gamma\delta\mathbf{g}$. Note that when the finite gradient approximation is made, \mathbf{q} is the area under the square gradient pulse in the PGSE experiment. Now, equation (3.8) can be re-written using the new variable \mathbf{q} .

$$E(\mathbf{q}, \Delta) = \int \rho(\mathbf{r}) \int P(\mathbf{r}|\mathbf{r}', \Delta) \exp(i\mathbf{q} \cdot [\mathbf{r} - \mathbf{r}']) d\mathbf{r}' d\mathbf{r} \quad (3.9)$$

In equation (3.11), the attenuation only depend on the dynamic displacement: $\mathbf{R} = \mathbf{r} - \mathbf{r}'$. Equation (3.11) can be further simplified by the definition of the average propagator \overline{P} :

$$\overline{P}(\mathbf{R}, t) = \int \rho(\mathbf{r}) P(\mathbf{r}|\mathbf{r} + \mathbf{R}, t) d\mathbf{r} \quad (3.10)$$

Equation 3.12 shows that the propagator is the probability that a particle displaces by \mathbf{R} over the time interval Δ . Applying both of these changes to eq (3.11) yields eq (3.13):

$$E(\mathbf{q}, \Delta) = \int \overline{P}(\mathbf{R}, \Delta) \exp(i\mathbf{q} \cdot \mathbf{R}) d\mathbf{R} \quad (3.11)$$

Equation 3.13 displays a Fourier transform relation between the between the echo signal and the propagator. By probing q-space with the PGSE experiment, spin ensemble displacements can be found in the form of a propagator, or distribution of displacements.

When there is no bulk flow in the sample equation 3.8 reduces to the Stejskal-Tanner relation for the attenuation of the echo amplitude [11, 25]:

$$E(g, \Delta) = \exp \left[-\gamma^2 g^2 \delta^2 D \left(\Delta - \frac{\delta}{3} \right) \right] \quad (3.12)$$

The Stejskal-Tanner relation shows that the signal attenuation at a certain gradient point normalized to the zero gradient point is a function of parameters of the pulse sequence, the gyromagnetic ratio, and the diffusion coefficient. Plotting the signal echo attenuation of multiple gradient points versus $-\gamma^2 g^2 \delta^2 \left(\Delta - \frac{\delta}{3} \right)$ on a semi-log plot and extracting the slope, which is the diffusion coefficient, is a very effective method of measuring self-diffusion coefficients precisely in equilibrated systems. The Stejskal-Tanner method for finding diffusion coefficients can be used for systems which do not display purely diffusive motion; for example stochastic motion which changes depending on the observation time scale, such as restricted diffusion and polymer reptation, and systems which display stochastic motion due to mixing, such as turbulence and dispersion[26][25]. In each of these cases, it is necessary to analyze the diffusion only over the gradient range which corresponds to 70 to 90 percent of the signal decay. The reason for this is that the probability of displacements to occur requires higher moments of the probability distribution function as it moves away from the mean displacement. Near the mean displacement, the probability of displacement will have Gaussian characteristics and can be more easily described with the second moment of the

probability distribution, which is the mean squared displacement of the molecules and corresponds with the diffusion coefficient. This will be elaborated on within the propagator formalism[11, 27, 28].

Velocity Imaging

Now that techniques for measuring both spin density in space and motions by measuring signal attenuation and phase shifts have been introduced, experiments that combine these techniques will be discussed. 2-D velocity imaging can provide valuable qualitative ideas on how fluids move through certain medias, such as the packed beds created in this thesis. This is essentially done by combining the motion tracking sequence and imaging sequence into one, and a phase shift is measured in each individual pixel.

Figure 3.4 shows this velocity imaging sequence.

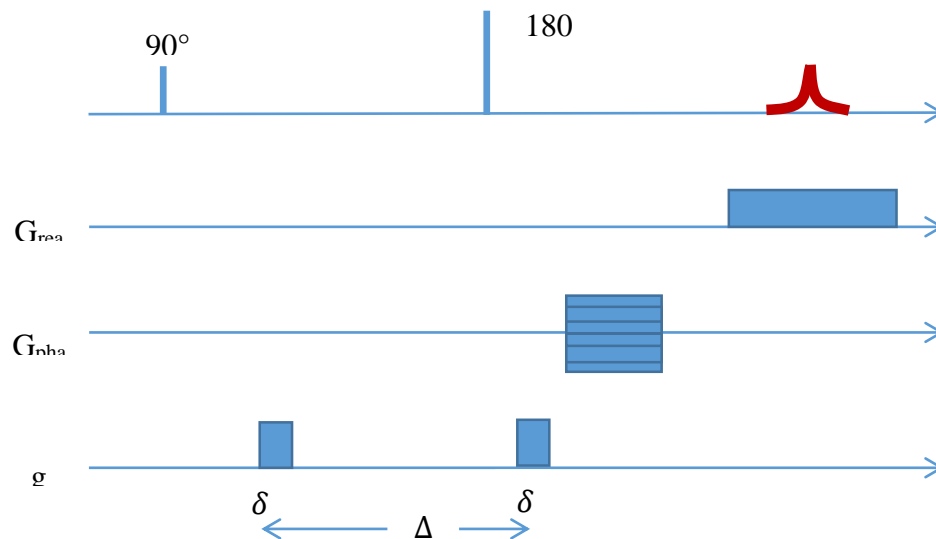


Figure 3.4: Velocity imaging sequence combines the spatial components of read and phase, with the encoding for initial and final position with g

This velocity sequence leads to a 2-D image in which the phase shift is measured in each pixel by the following equation:

$$v = \frac{\varphi_2 - \varphi_1}{\gamma(g_2 - g_1)\delta\Delta} \quad (3.14)$$

This sequence takes advantage of the basics of both k-space and q-space. It should also be noted that only two q points are found in each pixel, whereas a normal propagator usually steps through q space hundreds of times, again in with 2^n . Due to spatial resolution and lower signal to noise in images, higher averaging is usually required, and therefore 2-D velocity imaging generally takes large amounts of time, and is not useful for non-steady state flow systems.

CHAPTER 4: EXPERIMENTAL SETUP AND METHODS

A Pharmacia P-500 high precision pump was used to circulate fluid through a high pressure high performance liquid chromatography column (HPLC), with a 10 mm inner diameter, and a length of 50 mm. The chromatography column was wet packed with 235 μm , Duke Standards dry polymer microspheres. Fluid was pumped through the bead pack for at least 12 hours to eliminate air bubbles within the system.

Water experiments were run with 150 mL of deionized water, doped with Magnevist to reduce T_1 relaxation. After 12 hours of flowing, the column was transferred into the MR system, with the flow going from bottom to top. The flow through system of pump, tubing, and bead pack used was 40 mL, and was continuously circulated with a 110 mL water basin. Although the MR system has temperature control capability, the system was not changed from its 21 $^{\circ}\text{C}$ standard setting for water.

For CTAT experiments, approximately 150 mL of de-ionized water was measured out, and enough Hexadecyltrimethylammonium p-toluenesulfonate dry powder (Sigma Life Science) was added to create a 10.0 mM solution of CTAT. The solution was placed in a water bath of 25.0 $^{\circ}\text{C}$ right after the addition of powder, and the solution was stirred until dissolved then let to rest in the water bath for 24 hours. While keeping the sample within the water bath, the CTAT solution is pumped into the HPLC bead pack, and allowed to flow for 12 hours outside the MR system to eliminate air bubbles. The flow system is then loaded into the MR system, while keeping the solution basin in the water bath still set at 25 $^{\circ}\text{C}$. The temperatures of both the surrounding room, and the magnetic coil, are set to 25 $^{\circ}\text{C}$.

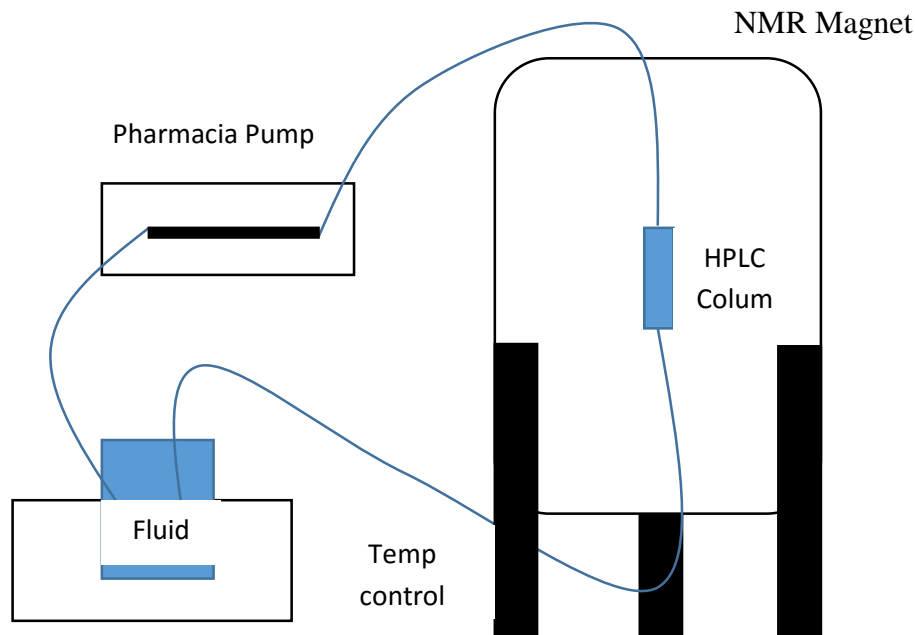


Figure 4.1: Model of entire flow setup while in the NMR magnet for each fluid.

For all solutions, many precautions were taken to avoid air bubbles in the column, as they cause artifacts in NMR results. All solutions were placed in a vacuum chamber for 1 hour before being pumped into the system. This was done to try and remove as much dissolved oxygen from the system that may potentially form air bubbles over time. Also, the beads were soaked with the fluid solution for several days before the HPLC column is constructed. This again is done to try and avoid air bubble build up.

For rheology experiments, a TA instruments AR series rheometer with a 2° cone and plate configuration was used for all solutions. Each solution is mixed for the same amount of time before measurements as they were for HPLC column loading, and then pipetted onto the rheometer sample surface. The shear rate is then steadily increased from 10 s^{-1} to 100 s^{-1} , and viscosity is measured. The sample is covered to help prevent

evaporation affecting chemical concentrations during experiments, and the sample is kept at a constant temperature of 25°C at all times.

NMR measurements used a Bruker AVANCE III spectrometer with a 7 T superconducting vertical wide bore magnet, Micro2.5 gradient imaging probe with a maximum gradient of 1.48 T m⁻¹ and 20 mm diameter radiofrequency (rf) coil.

CHAPTER 5: RESULTS AND DISCUSSION

Rheology Measurements

Due to CTAT's ability to combine into cylindrical micelles, complex viscoelastic behaviors can be observed. Using the AR series rheometer, the viscosity of CTAT at varying concentrations was tested with increasing shear rates.

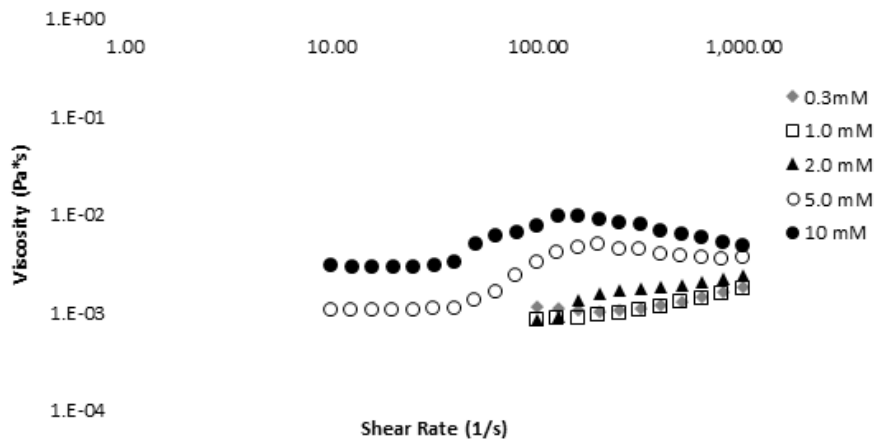


Figure 5.1: Apparent viscosity of CTAT solutions. Concentrations above the critical rodlike concentration (1.9mM) display a Newtonian plateau, with a shear-thickening regime where SIS formations occur, followed by a shear thinning regime where structures start to break down.

Above the CRC, CTAT show's interesting properties of having shear thickening, Newtonian, and shear thinning properties depending on applied shear rate. At lower shear rates, a Newtonian plateau is present. But as shear is increased, CTAT micelles are becoming larger and more entangled, forming shear induced structures (SIS) that cause shear thickening[1, 29]. As shear is increased further, the cylindrical micelle structures start to be pulled apart and align, causing the overall fluid to transfer into a shear thinning

regime, similar to common polymer fluids. It is important to note that 10 mM CTAT is the concentration used in all other NMR experiments, due to it having the largest amount of shear thickening behavior.

To calculate the apparent shear rate found within the bead pack used for MR experiments, the superficial velocity for 400 mL/hr flowrate was found [9]:

$$\langle v_{tube} \rangle = \frac{Q}{A} \quad (5.1)$$

where $\langle v_{tube} \rangle$ is the superficial velocity in a tube of equivalent dimensions of the beadpack, Q is the flowrate, and A is the cross sectional area of the column. Using this, the pore velocity is found:

$$\langle v_{pore} \rangle = \frac{\langle v_{tube} \rangle}{\phi} \quad (5.2)$$

where ϕ is the porosity of the column. This leads to an average pore velocity of 3.5 mm/s within each pore. The apparent shear rate in the porous media with spherical beads is [Bird]:

$$\gamma_{app} = \frac{\langle v_{pore} \rangle}{l} = \frac{\langle v_{pore} \rangle (1-\phi)}{d_p \phi} \quad (5.3)$$

This leads to an apparent shear rate of 21 s^{-1} for the flowrate and column used in this work, which would fall into the Newtonian plateau from figure 5.1. It is important to note that with a porous media's complex structure, simple shear conditions do not exist. This means that the applied shear rate on the fluid is highly dependent on the localized geometry. Reynolds number and Peclet numbers were also calculated to be 0.001 and 290, respectively.

$$Re = \frac{\rho \langle v_{pore} \rangle l}{\mu} \quad (5.4)$$

$$Pe = \frac{\langle v_{pore} \rangle l}{D_o} \quad (5.5)$$

Where ρ is the fluid density, μ is the viscosity, l is the characteristic length of the pore, and D_o is the self diffusion coefficient.

This means that the fluid is in the laminar regime, and advection is the dominate force [9, 30].

2D Velocity Images

Two dimensional velocity images were measured for water and 10 mM CTAT while flowing at 400 mL/hr. Black corresponds to zero velocity, and shows the position of solid beads, while red corresponds to the fastest velocities. The spatial distribution of velocities appear to be very similar between the two fluids, with mostly evenly distributed velocities and a few faster moving pores in red.

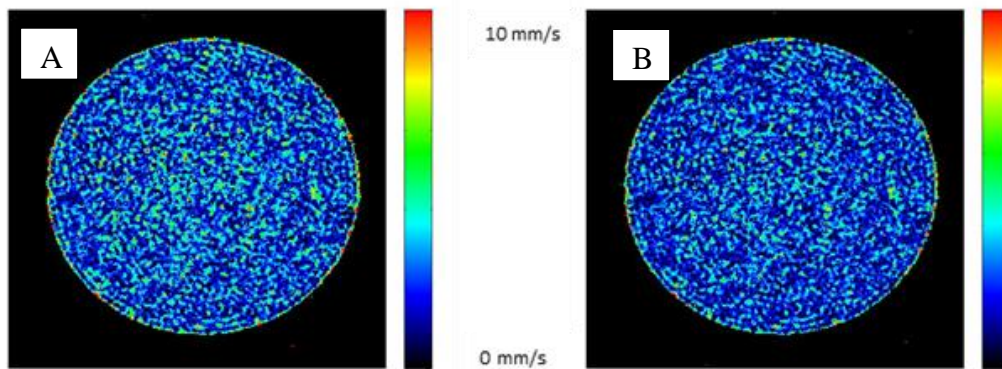


Figure 5.2: Cross sectional velocity images of 10 mM CTAT (A) and water (B) flowing in 10 mm inner diameter porous media with 250 μ m beads. Spatial resolution for each image is 55x55 microns per pixel, with 0.5 mm slice selection. Fluid flowrate was 400 mL/hr, with $\delta=0.5$ ms, $\Delta=9.5$ ms, $g_{max}=0.1360$ mT/m, 12 mm x 12 mm field of view, and 256x256 read and phase points.

To help quantify any differences in the velocity fields the average velocity and standard deviation were calculated for figure 5.2 A) and B). The average velocity for CTAT was found to be 3.5 mm/s, while water showed a slightly lower average velocity of 3.01 mm/s, with standard deviations of 0.13 and 0.09 mm/s respectively. Because of rheology differences with 10 mM CTAT, it would be expected that the flow field would show differences, but one possible problem could be arising in the above experiments. The resolution of the above images may not be fine enough to witness differences. Previous work was done with much beads larger than 1mm in diameter [15], but beads used in these experiments were 250 μm in diameter. With 55 μm resolution, 4 pixels would fit across a pore diameter, which may not be enough to detect changes in the velocity profile across a pore. 2D velocity imaging experiments take 24 hours to obtain data for one fluid, and increasing resolution would greatly increase the already long time of experiment. In this case, it is advantageous to use other methods to obtain information on pore flow profile.

Propagator Measurements

Propagator measurements were performed on both CTAT and water flowing through porous media at 400 mL/hr. Expected in theory, as well as shown in [31], as the observation time, or Δ , of water increases, the propagator distribution shifts towards a Gaussian shape, with its peak at the average velocity of the bulk fluid. Propagator measurements were made with Δ from 50 to 850 ms. Figure 5.3 shows the evolution into Gaussian distributions observed in these experiments. At 50 ms, the distribution is concentrated around zero displacement, due to the molecules not having enough time to

move. As observation time is increased, the molecules are allowed more time to move, and the distribution's peak moves toward a non-zero displacement. It should be noted that due to the process of random packing of the micro spheres, varying amounts of fluid would be trapped and not flowing in the porous media. This causes a spike of signal at the zero displacement point in the propagator.

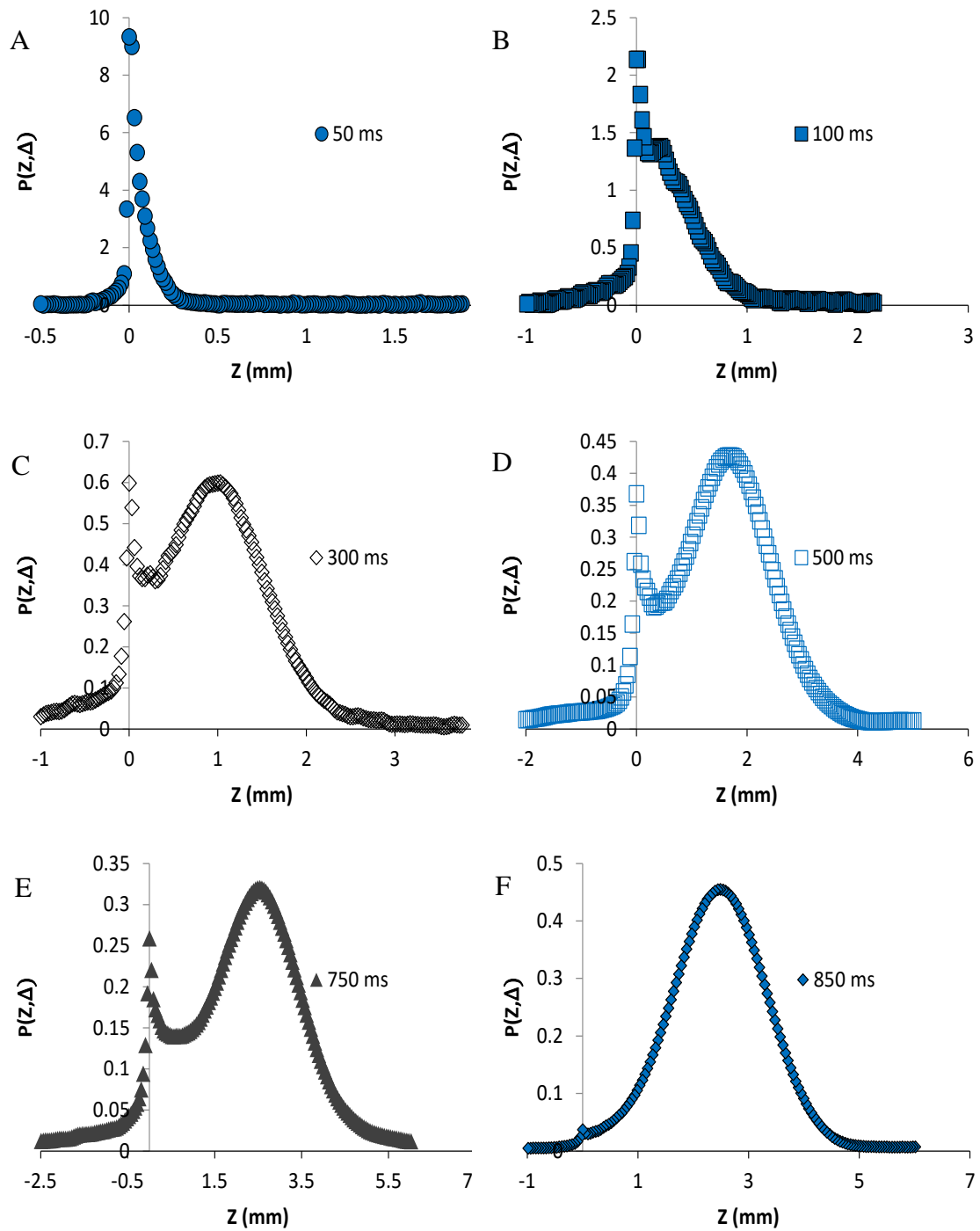


Figure 5.3: Propagator measurements for each observation time for water at 400 mL/hr. A) and B) show very little Gaussian behavior, but with longer observation times, a Gaussian shape takes form due to Δ being long enough that the motion has been averaged over several pore sizes.

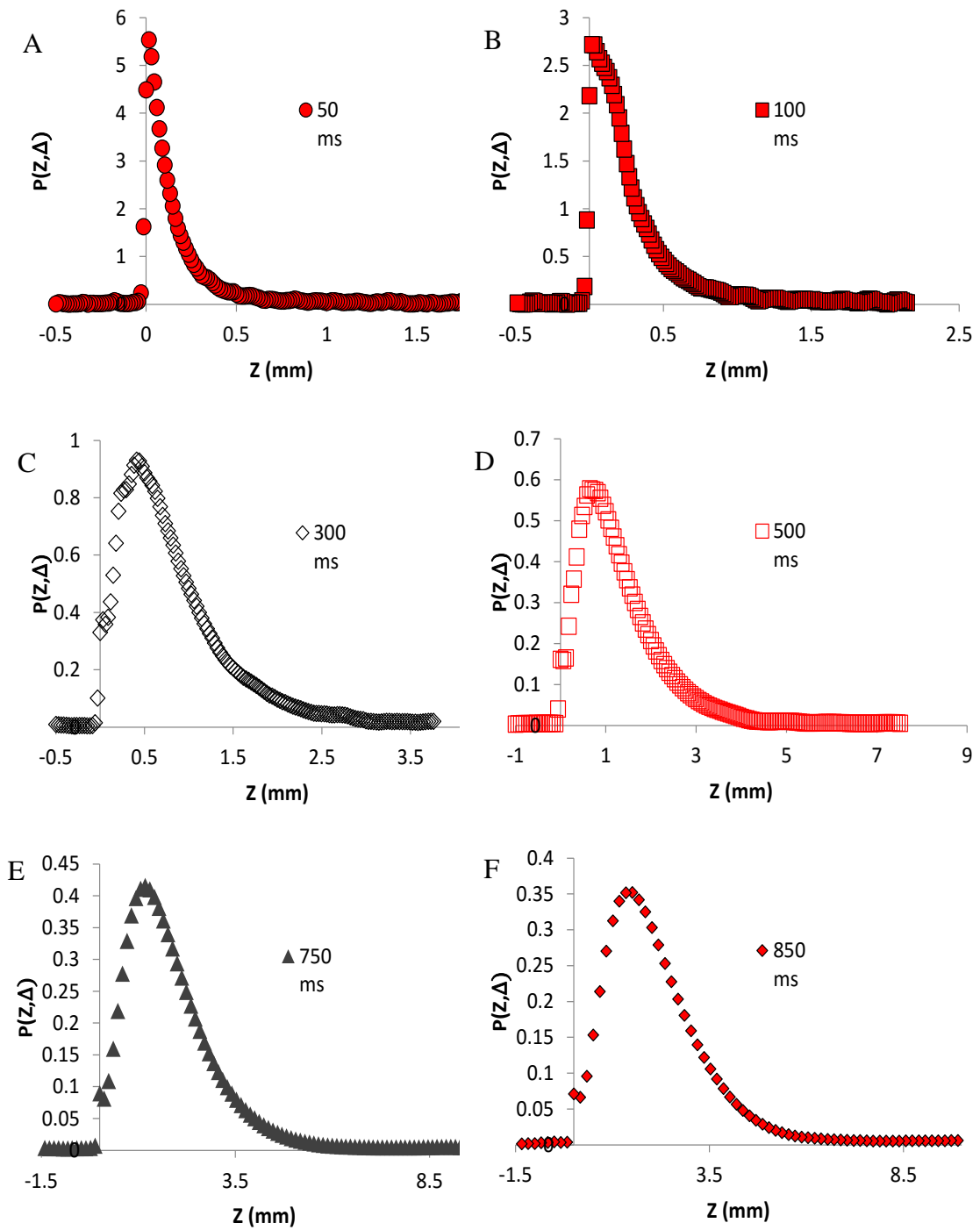


Figure 5.4: Propagator measurements taken at each time interval performed for CTAT. Due to the non-Newtonian nature of CTAT, a Gaussian shape is never achieved, with a long tail at large displacements

For CTAT, the evolution to a steady state shape is much slower, and long displacement tails can be seen as early as 300 ms. This is evidence that although the bulk of the fluid is moving at slower velocities, some pores are experiencing significantly higher velocities [15]. Both fluids are moving at the same volumetric flow rate, with the same cross sectional area in the column, but CTAT shows a much different distribution of displacements. Comparisons of these two fluids can be seen below.

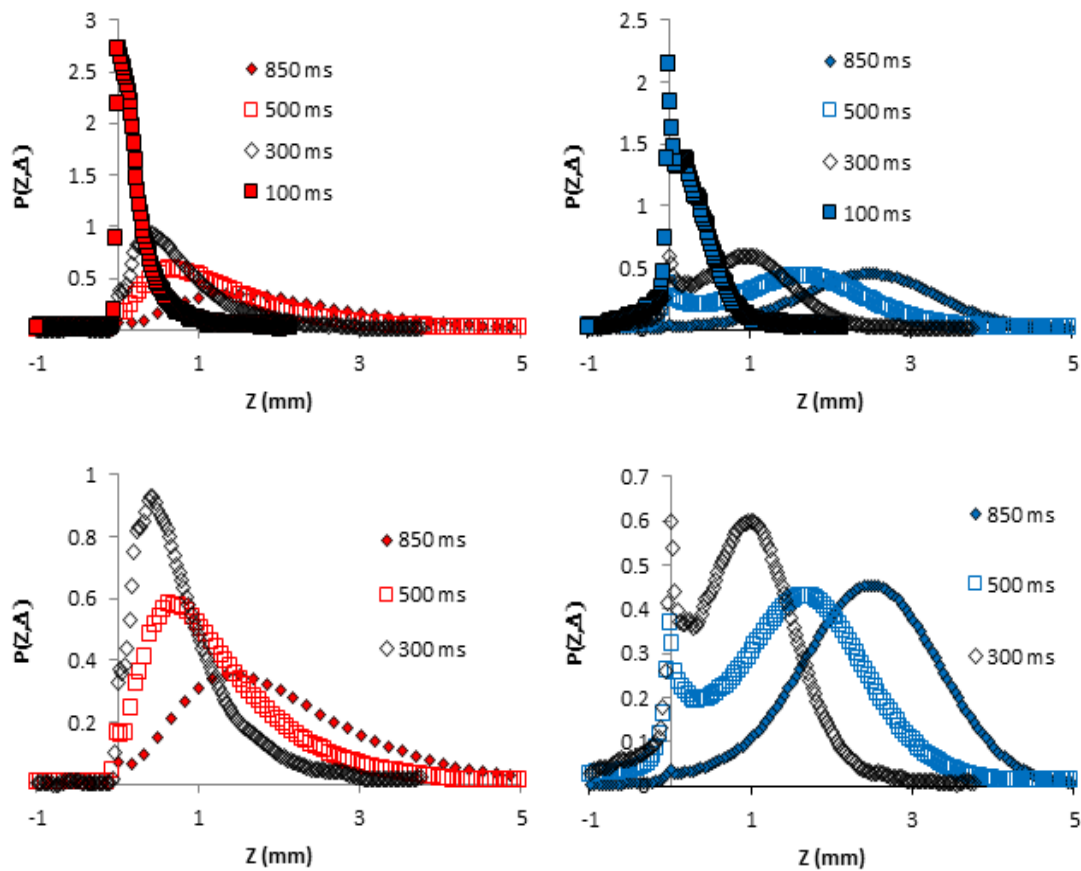


Figure 5.5: Propagator measurements. Propagator measurements. (A) CTAT for all Δ . (B) Water for all Δ . (C) CTAT for $\Delta=300, 500, \text{ and } 850$ ms. (D) Water for $\Delta=300, 500, \text{ and } 850$ ms.. Water shows an evolution towards a Gaussian shape at longer observation times, whereas CTAT shows an evolution towards a non-Gaussian shape with longer tails.

To help quantify the non-Gaussian shape of CTAT, the third moment of the probability distribution, or skewness, of each propagator was found. An increasing skew results from shifting the max of the propagator towards smaller displacements, and longer tails at higher displacements. For 850 ms, CTAT and water show a skew of 3.63 and 1.24, respectively. The below table shows the skews at the longest observation times[32].

Table 5.1 : Skews calculated for CTAT vs. water at longer displacement times. CTAT uniformly has a larger skew than water, leading to quantitative evidence that CTAT consistently shows longer tails with a non-Gaussian propagator.

	CTAT	Water
300 ms	2.86	1.33
500 ms	2.43	1.78
850 ms	3.63	1.24

The observation of long tails for a non-Newtonian could be expected in shear thinning fluids. As the fluid experienced shear forces within a pore, the fluid would have less and less resistance due to the lowering viscosity. As the viscosity lowers, the fluid would move faster and faster through that individual pore. This would lead to preferential pores where fluid moves faster through a few pores, while the fluid moves slower through others. These preferential pathways would have higher displacements in the propagator, and therefore lead to long tails in the propagator [ref]. As discussed above, the expected shear in the bead pack would put CTAT into the Newtonian regime, but this calculation doesn't account for the tortuous path the fluid takes through the network, or the normal forces that could be applied to the fluid due to the tortuous path. This could lead to the

fluid going through a large array of shear rates in the porous media, and measurements for CTAT could come from Newtonian, shear thickening, and/or shear thinning regime[33, 34] [35, 36].

Dispersion Measurements

To help further quantify the non-Gaussian nature of CTAT, the approach of Guillon et al [37] was to measure dispersion. A criteria of Δ above 1.22 seconds was used to make sure all of the pore space is sampled, as measurements need to be in the asymptotic regime. This was found by using the criteria:

$$\sqrt{2D_o t} > 0.3d_g \quad (5.4)$$

Where D_o is the self-diffusion coefficient and d_g is the bead diameter. Experiments of Δ varying from 1.3 ms to 1.9 ms were run to analyze dispersion within the bead pack for both fluids. Collection techniques similar to the Stejskal-Tanner relation were used, but the attenuation q-space data was analyzed [25] [11]. Q-space, and not displacement, was analyzed to avoid any problems that could occur with fourier transforming the data. In the asymptotic and Gaussian regime, standard deviation of the displacement, or the variance of displacement, scales linearly with observation time. Sub, or super dispersion is characterized with a power law scaling[37, 38].

$$\sigma^2 \propto \Delta^\alpha \quad (5.5)$$

To find the relationship between signal and variance, equation (3.9) is modified to give:

$$\ln|E(q, \Delta)| = -\frac{1}{2}\sigma^2 q^2 \quad (5.6)$$

The resulting variance of displacement (σ) was found for each observation time, and plotted on a log plot vs Δ . The power law, α , was then found for each fluid.

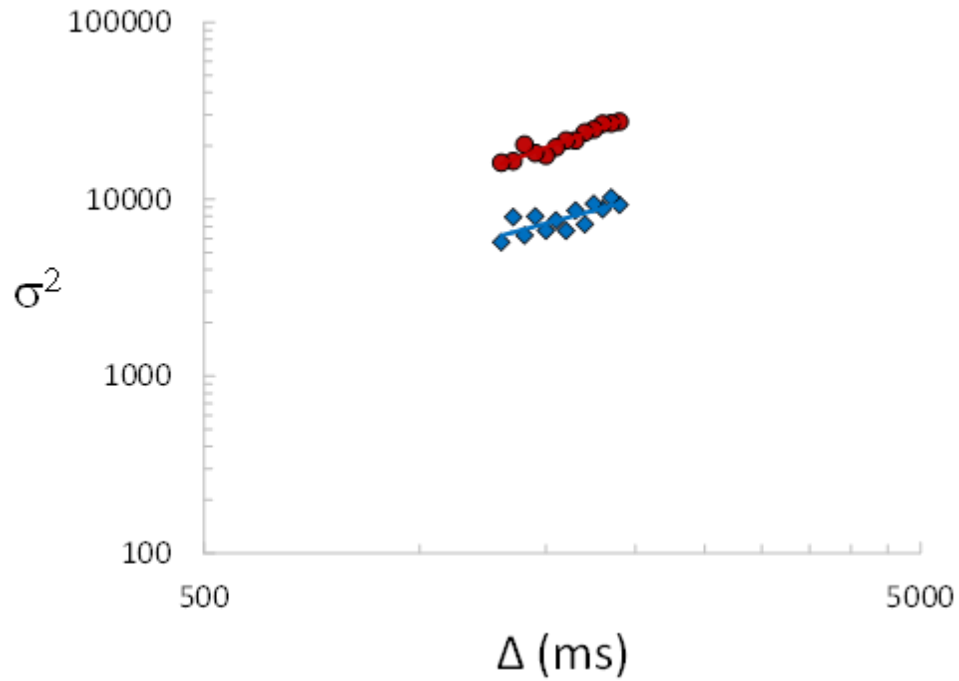


Figure 5.6: Variance of the displacement vs. observation time. The power law exponent $\alpha = 1.1$ for water and $\alpha = 1.45$ for 10 mM CTAT.

Observations made with propagator measurements, along with other work with propagators in porous media [21, 39, 40], have shown that in the asymptotic regime, a Gaussian distribution displacements is observed in water. A power law difference of $\alpha = 1.1$ to $\alpha = 1.45$ when comparing water to CTAT shows that the WLM are display super-dispersion properties within the porous media.

According to Saffman[41, 42], dispersion with the limitation:

$$Pe = \frac{\langle v \rangle l}{D_o} \ll 1 \quad (5.7)$$

follows Taylor dispersion, where longitudinal dispersion is increased with shear in flow. Pe scales with dispersion by a power law Pe^β , where $\beta=1$ for situations in which velocity variations cause dispersive effects, and $\beta=2$ for diffusion being the dominant effects [43]. For CTAT, in which transport in the porous media is anomalous compared to water, Pe number scaling would be very difficult to predict due to WLM changing the dispersive forces acting upon the fluid[44-47].

Conclusion

Data collected from 2-D velocity images showed slight evidence of flow profile changing when comparing water to CTAT, but by using PGSE NMR, changes were witnessed by measuring displacements of spin isochromats. Propagator measurements, along with measured skew, showed that CTAT displays a non-Gaussian distribution, with long tails in higher displacements. Dispersion experiments showed that non-Gaussian CTAT changes the power law scaling from Gaussian scaling in σ vs Δ when experiments are analyzed in the non-Fourier transformed q -space.

This gives a small amount of insight into how WLM's complex rheological properties change the fluid's transport in porous media. Much more experimentation is needed to fully understand the mechanisms by which the WLM's cause non-Gaussian behavior, and how it can be tied to the fluid rheology.

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